

In the claims:

The following list of claims replaces all preceding lists of claims.

1. (original) A process for the conversion of sewage sludges, the process characterized by the steps of:
 - (a) feeding dried sludge through a reactor;
 - (b) heating the dried sludge in the reactor in the absence of oxygen for the volatilization of oil producing organic materials therein, resulting in gaseous products and sludge residue;
 - (c) transferring the gaseous products from the reactor to a catalytic converter;
 - (d) contacting the gaseous products from the reactor or the reheated oil and/or non-condensable products, if any, with a catalyst in the catalytic converter in the absence of oxygen;
 - (e) removing the gaseous products from the catalytic converter; and
 - (f) condensing and oil/water separating the gaseous products of the catalytic converter.
2. (original) A process according to claim 1, wherein sludge residue from the reactor is transferred to a storage bin through a valve system for ensuring both no air ingress into and no gaseous product egress from the reactor.
3. (original) A process according to claim 1 or 2, wherein the feeding of the dried sludge through the reactor utilizes a feed system that ensures both no air ingress into, and no escape of gaseous products from, the reactor.
- 4 (currently amended) A process according to claim 2 or 3, wherein the temperature of the reactor is at least 250°C.
5. (original) A process according to claim 4, wherein the temperature of the reactor is about 450°C.
6. (currently amended) A process according to ~~claim 1 any one of the preceding claims~~, the process further characterized by the method steps of:
 - (g) transferring the gaseous products from the reactor to a condensation system to condense the oil product from the gaseous products; and
 - (h) reheating water free oil and/or non-condensable products, if any, from the condensation system in an oil reheater.
7. (currently amended) A process according to ~~claim 1 any one of the preceding~~

claims, wherein the condensation system of step (f) comprises direct condenser.

8. (original) A process according to claim 6, wherein the condensation of step (g) comprises indirect condensation at $> 100^{\circ}\text{C}$.

9. (currently amended) A process according to ~~claim 1 any one of the preceding~~ claims, wherein the direct transfer of gaseous products of step (b) from the reactor to the catalytic converter takes place in heat traced lines.

10. (currently amended) A process according to ~~claim 1 any one of the preceding~~ claims, wherein the temperature of the catalytic converter is up to 650°C , thereby promoting reductive, catalytic gas/solid phase reactions and substantially eliminating hetero-atoms, including nitrogen, oxygen, sulphur, and halogens.

11. (original) A process according to claim 10, wherein the catalytic converter temperature is in the range of 400 to 550°C .

12. (currently amended) A process according to claim 10, wherein the catalytic converter temperature is in the range of 400 to 420°C

13. (currently amended) A process according to ~~claim 1 any one of the preceding~~ claims, wherein the catalytic converter contains a catalyst, the catalyst being chosen from any of zeolite, activated alumina, γ -aluminium oxide, silicon oxide and oxides of alkali, earth alkali and transition metals.

14. (original) A process according to claim 13, wherein the catalyst is zeolite.

15. (currently amended) A process according to ~~claim 6 any one of claims 6 to 14~~, wherein the process further comprises the step of testing the miscibility of the oil product with a hydrocarbon solvent and modifying the conditions of the catalytic converter in response thereto.

16. (currently amended) A process according to ~~claim 6 any one of claims 6 to 15~~, wherein the oil product of the process is miscible with a hydrocarbon solvent.

17. (original) A process according to claim 16, wherein the solvent is diesel fuel.

18. (currently amended) A process for the conversion of sewage sludges, the process characterized by the steps of:

- (a) feeding dried sludge through a first reactor;
- (b) heating the dried sludge in the first reactor in the absence of oxygen for the volatilization of oil producing organic materials therein, resulting in gaseous products and sludge residue;

- (c) transferring gaseous products from the first reactor to a first condensation system;
- (d) transferring sludge residue to a second reactor where it is heated with oil and/or non-condensable products from the first condensation system;
- (e) transferring the gaseous products of the second reactor to a catalytic converter;
- (f) contacting the gaseous products of step (e) with a catalyst in the ~~catalytic catalyst~~ converter in the absence of oxygen;
- (g) removing the gaseous products from the catalytic converter; and
- (h) condensing and oil/water separating the gaseous products of the catalytic converter.

19. (currently amended) A process according to claim 18, wherein the temperature of both reactors is ~~about~~ about 450°C.

20. (original) A process according to claim 18, wherein the catalytic converter has a temperature of about 400 to 420°C.

21. (original) An apparatus for the conversion of carbonaceous materials, the apparatus characterized by a feed system for dried material to be conveyed, a reactor, and a catalytic converter, the reactor having a solid product discharge outlet and a transfer line provided for transport of gaseous product directly or indirectly to the catalytic converter.

22. (original) An Apparatus according to claim 21, wherein a first condensation system is provided in-line between the reactor and catalytic converter.

23. (original) Apparatus according to claim 22, wherein the first condensation system includes an oil/water separation system.

24. (currently amended) Apparatus according to ~~claim 21~~ any one of claims 21 to 23, wherein the catalytic converter is adapted to contact heated catalyst contained therein with oil or oil and non-condensable products of the condensation system, wherein gaseous products may be removed from the catalytic converter.

25. (currently amended) Apparatus according to ~~claim 21~~ any one of claims 21 to 24, wherein a reheater is provided between the first condensation system and the catalytic converter.

26. (currently amended) Apparatus according to ~~claim 19~~ any one of claims 19 to 25, wherein a second condensation system is provided to receive gaseous product from the catalytic converter.

27. and 28. (cancelled)